

Risk assessment methodologies of hydrogen applications in a socio-technological context

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New technologies have to be at least as safe as the well known alternatives.

Testing and systems analysis is required to achieve high level of safety

The lecture is dealing with methodologies that describe the hydrogen applications as being part of a socio-technological system.

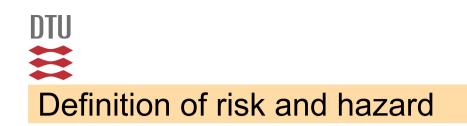


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DTU Outline of lecture

- Accident model, scenarios, basic measures
- The role of risk analysis
- Hazard identification
- Functional modelling
- Barrier diagrams
- Short about GIS-systems
- Uncertainty in the results







The "Seveso-II-directive" includes definitions for hazard and risk:

<u>Hazard</u> shall mean the intrinsic property of a dangerous substance or physical situation, with a potential for creating damage to human health and/or the environment.

<u>*Risk*</u> shall mean the likelihood of a specific effect occurring within a specified period or in specified circumstances.

As such,

<u>RISK</u> is a complex function of:

•the *hazards* connected with a certain system,

•the probability that a hazard results in an undesired event,

•the consequences of this event and

•the *vulnerability* of the environment that is exposed.

 <u>Perceived risk</u>, or risk as interpreted by the general public, as well as the <u>acceptability of certain risks</u> appear to depend on many aspects like control, dread, knowledge and trust.



Historical development of Risk Analysis



Of methodologies and techniques for complex systems

1. <u>Technical age:</u>

 Fokus on operational & engineering methods to "combating" hazards

2. <u>Human error age</u>:

Human beings are capable of circumventing even the most advanced engineered safety device

3. Socio-technical age:

Recognition that the major residual safety problems do not exclusively belong to technical or operational factors, but that the interactions between the technical and social aspects of the system are important

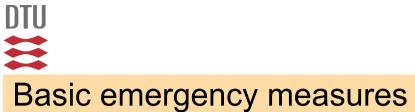




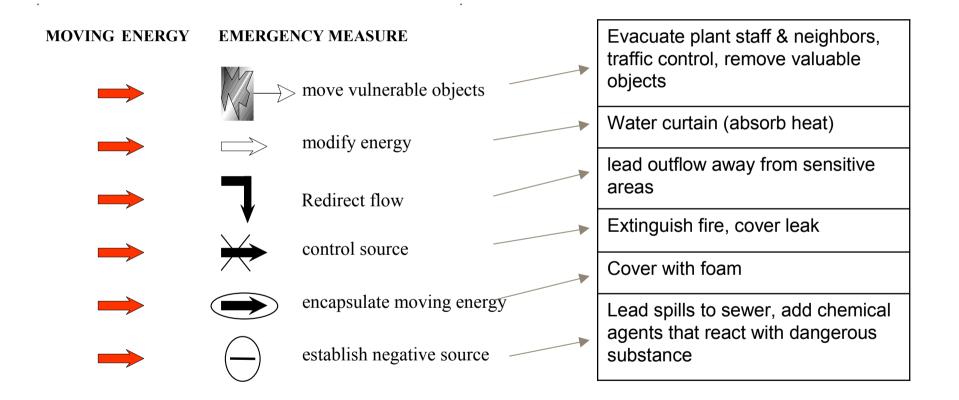


SOCIO-TECHNICAL CONDITIONS USUBLE SOURCE USUBLE SOURCE OF USUBLE SOURCE O











A GENERAL ACCIDENT MODEL



Any accident can be described as one or more sequences of "energy transfer", influenced by more or less successful confinements.

•A confined amount of energy can constitute a <u>hazard source</u>. If sufficient energy is present, the prerequisites for an accident are present. It is essential to ensure that all hazard sources of the considered activity are identified and evaluated.

•Central factors of the model is <u>confinement</u> and <u>loss of confinement</u>. Confinements involve containing systems and control systems. In order to control the hazard source possibilities for confinements must be identified and realised.

•The combination of sufficient energy and inadequate confinement results in <u>uncontrolled flow of energy</u> (UFOE).

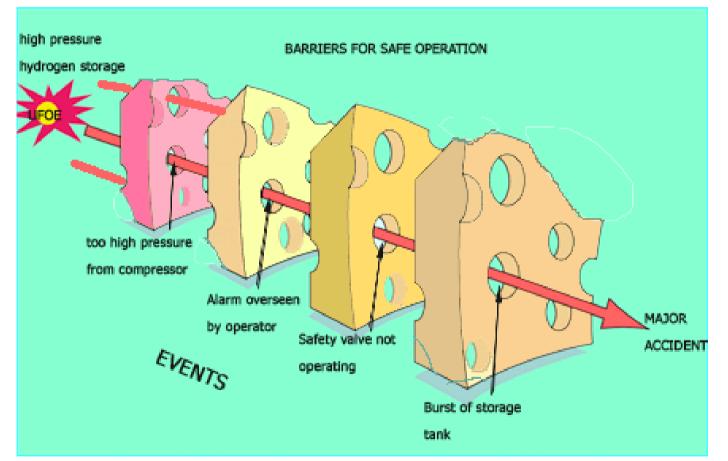
•If a <u>vulnerable object is exposed</u> to an energy flow without sufficient barriers then the accidental consequence becomes a fact. There is a near-miss incident if a UFOE occurs without hitting a vulnerable target. Vulnerable objects can be human beings, environment and property.



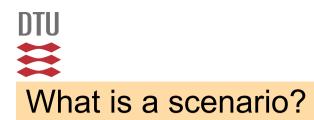


Barriers & Events Swiss-cheese model









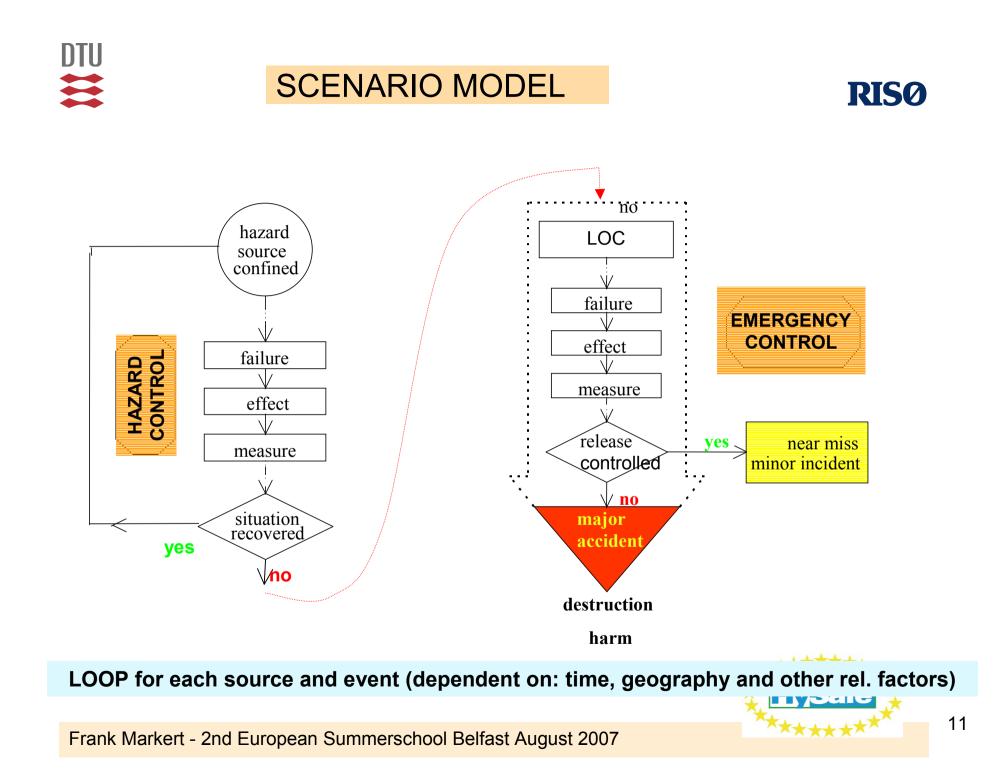


An Accident is a specific, unplanned sequence of events

For each EVENT the following has to be analysed:

- **FAILURE:** Not intended condition or event
- **EFFECT:** Consequences, impact, change-of-state, change-of-condition, domino effects, failure propagation
- **MEASURE:** Protective, preventive, operation, equipment, decision, alarm





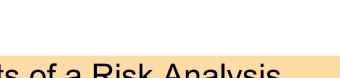


SCENARIO MODEL - TABLE



loop	failure	effect	measure
0	-	-	storage conditions, smoke/gas detectors and alarms, packing materials, facility
1	insufficient storage tests, temperature too high	wrong storage conditions, decomposition, heat generation	smoke detection
2	smoke detection too slow	escalation of decomposition, damage to packing materials	fire alarm
3	release of burning chemicals	domino effect, ignition of part of the storage	on-site emergency operation (extinguish fire, cover with foam)
4	bad access to fire source	insufficient fire fighting, developing fire	on-site emergency operation (extinguish fire, cover with foam), alarm to police and fire brigade
5	fire fighting insufficient	fully developed fire, damage to building, release of toxic fumes	evacuate plant staff, evacuate neigh- bours, stop traffic to area, remove valu- able objects
6	evacuation too slow	harm to people	hospitals, ambulances
7	insufficient collection of water from fire fighting	contamination of recipients	cleaning of contaminated areas
8	fire fighting insufficient	damage to property	build new storage

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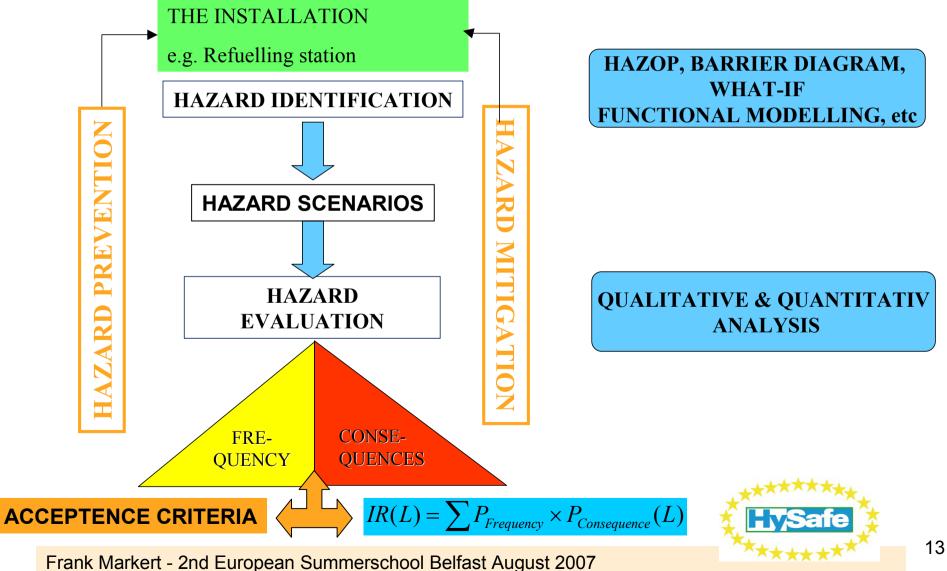




Elements of a Risk Analysis

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DTU HAZARD IDENTIFICATION

- Methods based on a <u>top-down analysis</u>,
 - start from a top event and going down to basic events
 - e.g. Fault Trees, Functional analysis, Hazard and Consequences Analysis
- Methods based on a <u>bottom-up analysis</u>,
 - starts with deviations of the process variables/failures of devices investigating the consequences
 - e.g. HAZOP, Structured What-If Technique (SWIFT), Hazard Screening Analysis (HAZSCAN) and FMEA
- Methods based on the <u>systematic use of standard</u> <u>checklists</u>, after division of the plant in areas, lessons learnt from past accidents/detailed studies.

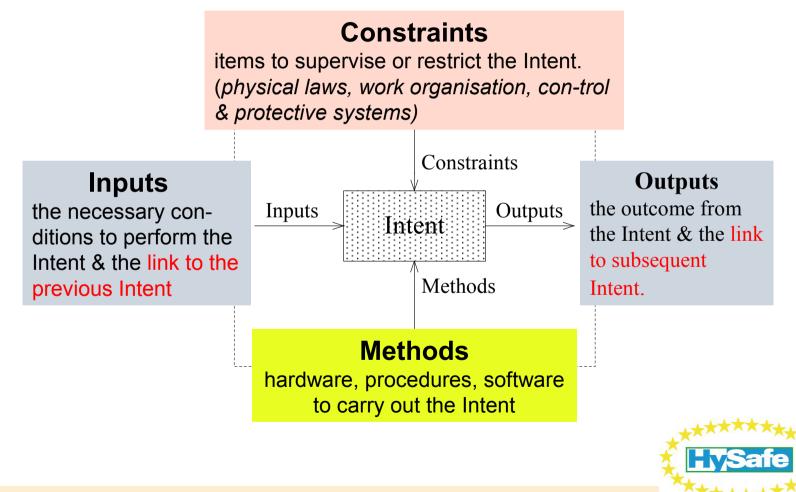




HAZARD IDENTIFICATION Functional modelling – basic object



Intents - the functional goals of the specific plant activity



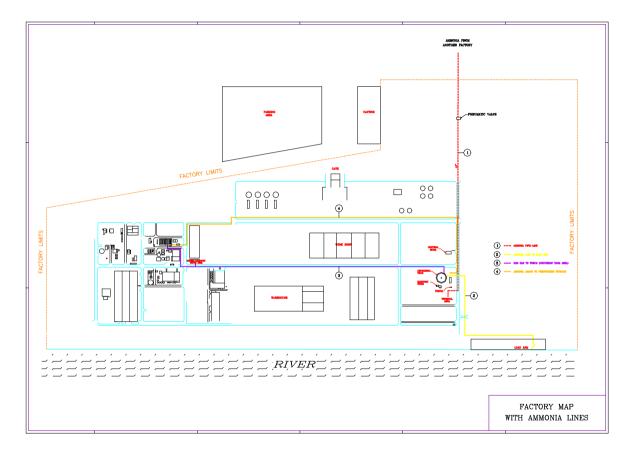
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An example – large gas storage

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INSTALLATIONS:

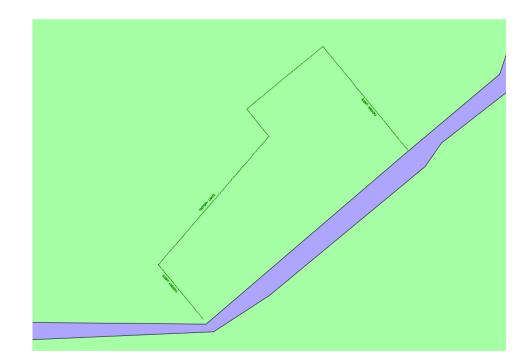
Pressurized storage Cryogenic storage Pipelines (delivery) Pipelines (connecting)



DTU Example plant subdivision into functions 1

F0

gas storage facility





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DTU Example plant subdivision into functions 2

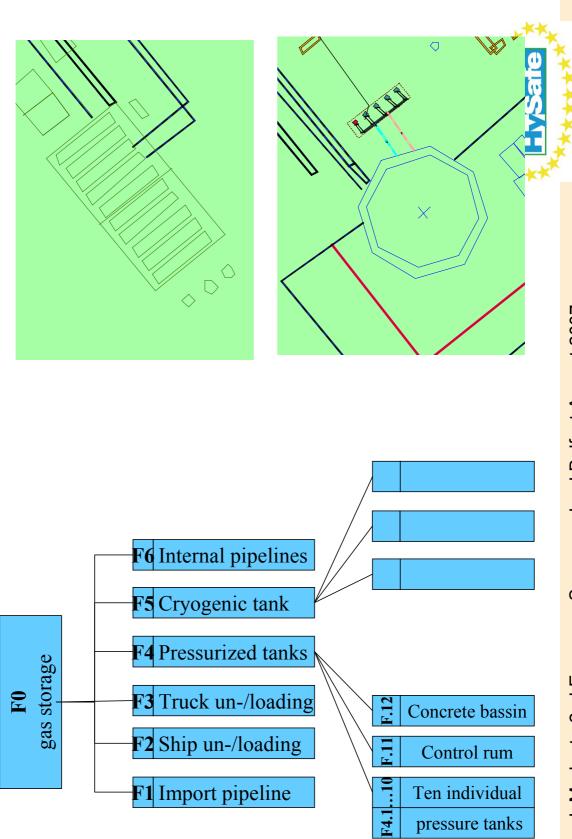


FO Ammonia storage F4 F3 F1 F2 F5 F6 **F2 F3 F4 F5 F6** F1 Ship Internal pipelines Truck un-/loading Import pipeline Pressurized tanks Cryogenic un-/loading tank



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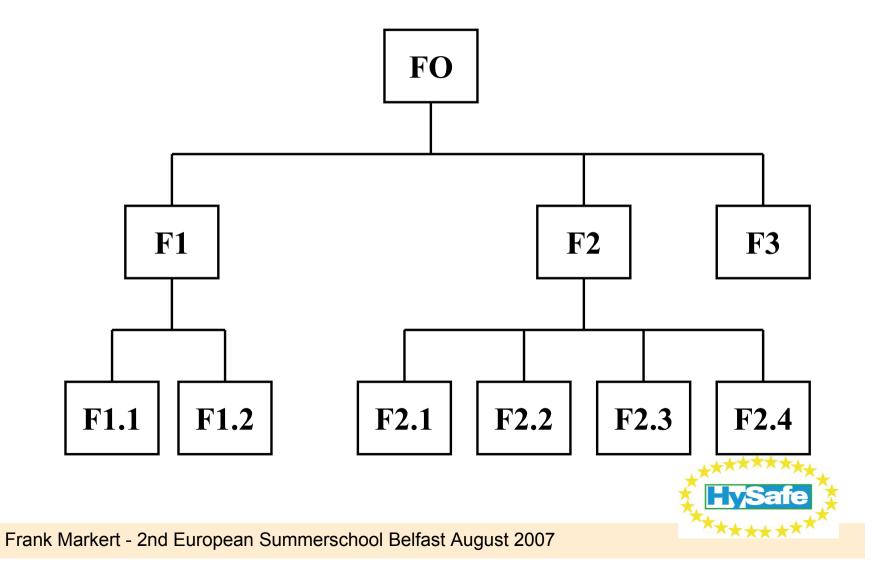




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DTU Hazard identification – Functional modelling



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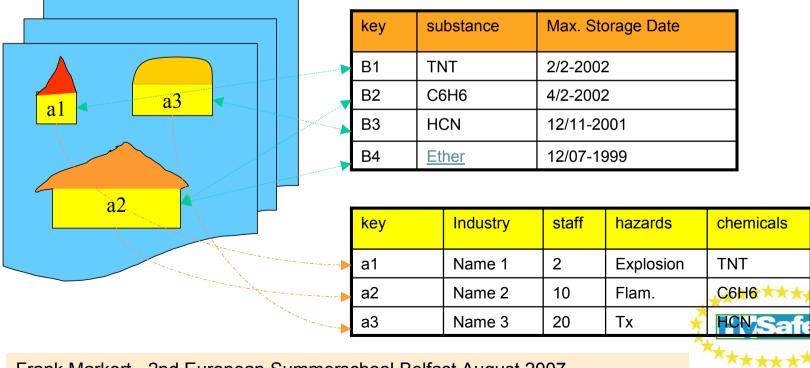
Output example for functional modelling

Intent		Storage of chemicals
Methods	Safety	Alarms (e.g. gas, smoke)
		Fire engines and equipment
	Operation	Coordination of activities
		Safety culture
		Maintenance and repair
		Construction
		Inspection
		Manuals, procedures and instructions
Constraints	straints Safety Prevent fire ignition	
		Manage fire
		Manage exposure
		Protect storage from external damage
	Operation	Logistics
		Inspection and supervision
		Manuals, procedures and instructions

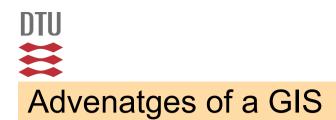


DTU What is a Geographical Information System?

- Database
- Map
- Advanced analysis of data linked to geographical information
- Data management system



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- GIS database will preserve the geographical data
- Visualisation of exact locations of the equipments.
- Easier to assess possible domino effects
- Application of (regional) maps
- Correlation with population densities or vulnerable environments etc. to supports the analyses of the consequences,
- Present IR curves around the facility or to calculate more easily F-N curves.



DTU BARRIER DIAGRAMS



Barriers can be defined as measures present to interrupt an accident event sequence,

(i.e. prevent the end-event of the accident scenario in occurring.)

Examples of barriers:

•An alarm for instance for high level in a tank.

•A sprinkler system in a building to prevent fires in developing.

•A dike surrounding a tank, designed to contain accidental spillage from the tank.

Barriers can be of different types.

- •Active versus passive barriers
- •Automatic versus manual barriers







Barrier diagrams serve two main purposes:

1) Evaluation of adequateness of safety measures (part of accident prevention)

(Are the barrieres reasonable and independent? Are barriers missing?)

2) Communication to all stakeholders

(Illustrating the possible accident scenarios and safety measures taken to prevent them)



CONSTRUCTION OF BARRIER DIAGRAMS

The construction of barrier diagrams consists of 4 steps:

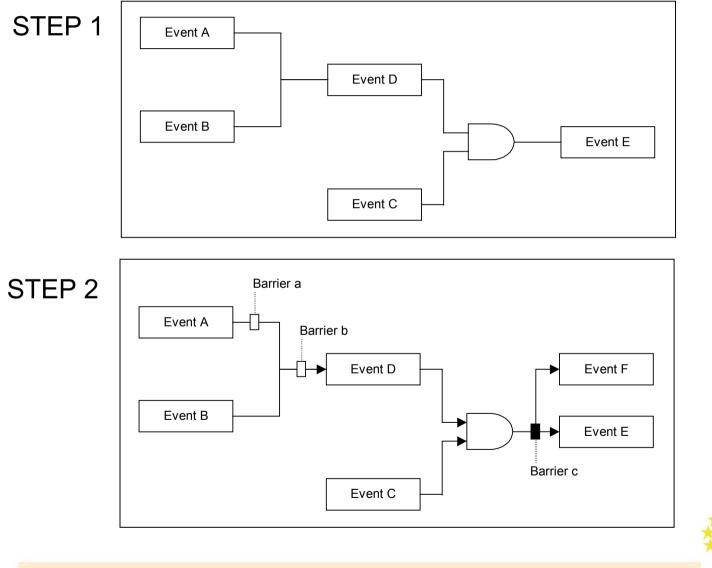
- 1. Construction of the event chains
- 2. Inclusion of the barriers.
- 3. Evaluation for each barrier of what would happen assuming that the barrier is effective and construction of relevant event chains from the evaluation.
- 4. Classification of barriers according to type or evaluated reliability of the barrier (optional).

When constructing barrier diagrams one must start with ignoring all the existing barriers! The main structure of the barrier diagram is the event chains, which may consist of elements from both the event tree and the fault tree method. An example the event (cause-consequence) chains of a barrier diagram is given below. The events most to the left may be called the initiating events (causes) and those most to the right the consequences.



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DTU RISO STEPS IN CONSTRUCTING BARRIER DIAGRAMS







Evaluation of barrier diagrams

- Once the barrier diagram is finished, the level of safety should be evaluated.
- The purpose of evaluating the barrier diagrams is to determine whether there are sufficient barriers against the undesired events happening, i.e. is the design sufficiently safe.

When evaluating the diagram one must consider:

- The frequency/probability of the initiating events
- The severity of the end events (consequence assessment)
- The number, coverage and reliability of barriers in each of the event chains in the diagram







• <u>Aleatory</u>, also known as stochastic uncertainty or due to randomness.

This can be called irreducible. Even if a certain narrowing of the range in which the risk figures are defined can be achieved through a better knowledge of their distributions, quantities such as failure rates, and meteorological conditions at the time of a release, size of a breakage etc. can only be defined through probability distributions.

Aleatory uncertainties can be treated by well-established methods, e.g. propagated through the analysis by Monte Carlo simulation.

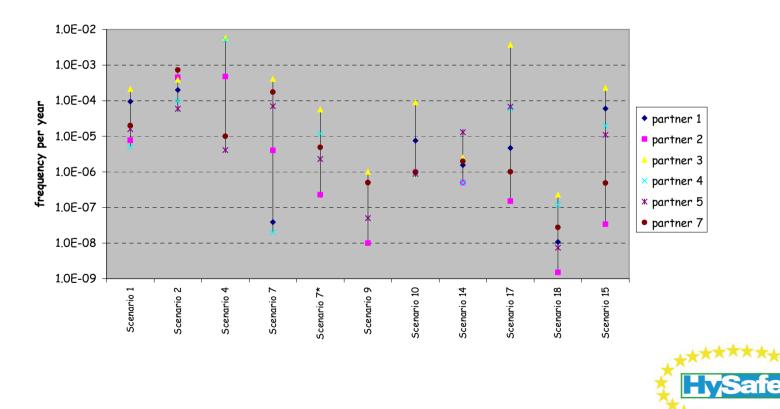
• <u>Epistemic</u> (also called reducible uncertainty) is related to incomplete knowledge about phenomena of concern and inadequate matching of available databases to the case under assessment, etc.







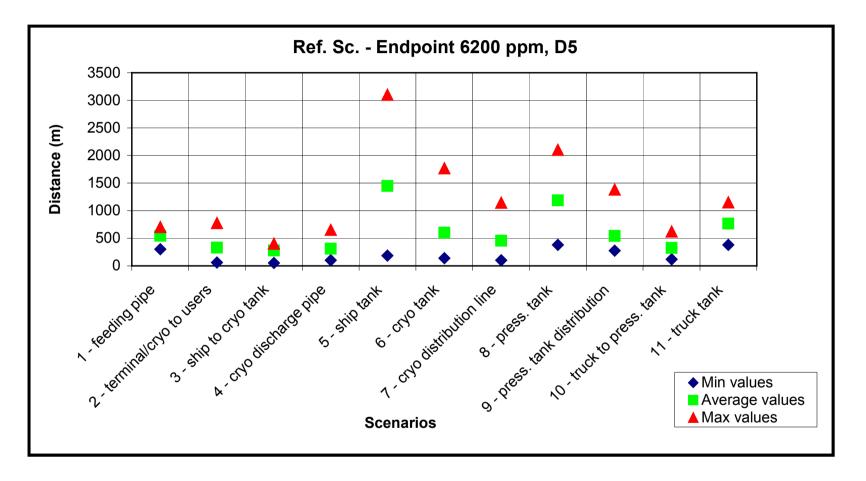
The EU ASSURANCE project - Sources and magnitudes of uncertainties in risk analysis of chemical establishments



Frequencies - pipeline related scenarios

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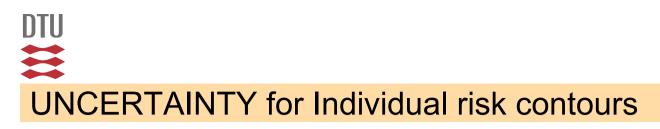
DTU UNCERTAINTY for CONSEQUENCES I



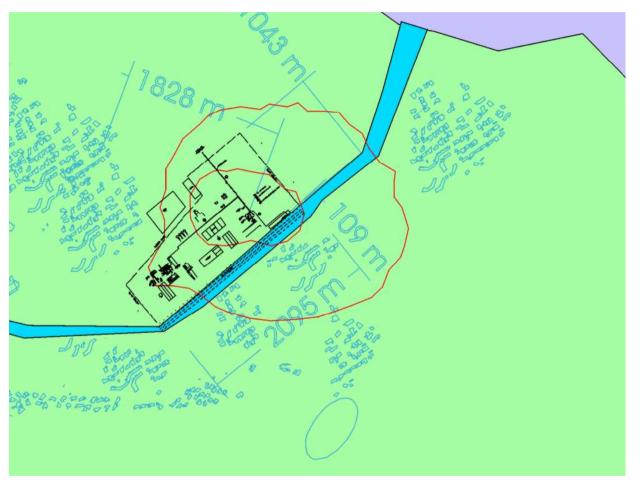


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Min - max for IR = 10^{-5} per year



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UNCERTAINTY IN COMMUNICATION Ranking - Frequencies

Partner	category 1 range (year ⁻¹)	category 2 range (vear ¹)	category 3 range (year ⁻¹)	category 4 range (year ⁻¹)	category 5 range (year ⁻¹)
1	improbable	remote	occasional	probable	
	$< 10^{-6}$	$< 5 \times 10^{5}$	$< 10^{3}$	$<5 \times 10^{2}$	
2	very unlikely	unlikely	likely	very likely	
	$< 10^{9}$	$< 10^{7}$	$< 10^{5}$	$< 10^{3}$	
3	1	2	3	4	5
	$< 10^{-2}$	$<3 \times 10^{2}$	$< 10^{1}$	<1	>1
4	significant				
	>109				
5	very low	low	medium	high	
	$< 10^{6}$	$< 10^{5}$	$< 10^{4}$	$>10^{4}$	
7	extremely	very unitkely	unlikely	likely	probable
	unlikely		-	-	-
	< 10 ⁻⁵	$< 10^{4}$	$< 10^{-3}$	$< 10^{2}$	$> 10^{-2}$

Range of "labels" assigned to a frequency of 10⁻⁵ /year



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UNCERTAINTY IN COMMUNICATION Ranking - Consequences

Partner	category 1	category 2	category 3	category	category 5	
1	marginal transitory	dangerous injuries/minor	critical	catastrophic injuries/		
	health problem/damage	damage inside the plant	minor injuries outside the	severe damage outside		
	inside the plant		plant. Fatalities/major	the plant		
			damage inside the plant			
2	<u>class 4</u>	class 3	<u>class 2</u>	<u>class 1</u>		
	no fatalities consequences	some fatalities cons 100 –	minor fatalities cons.	many fatalities		
	< 100m	500 m	<u>>500 – 1000 m</u>	consequences> 1000 m		
3						
	rate $< 3 kg/s$	$3 - 10 \ kg/s$	$10 - 30 \ kg/s$	30–100 kg/s	>100 kg/s	
	release < 3 min	3 <i>–10 min</i>	10 – 30 min	30–100 min	>100 min	
4	a large number of release categories have been defined					
5	minor	severe	<u>major</u>	<u>catastrophic</u>		
	on-site effects only	injuries offsite	few fatalities offsite	many fatalities offsite		
6	ordered after: length of reversible effect thresholds and max effect distances					
7	negligible	low	medium	<u>high</u>		
	$< 0.5t NH_3$	0.5 - 5 t	5 - 50 t	$> 50 t NH_3$		

Definitions of a catastrophic event





Sources for uncertainty

- the implicit or explicit assumptions about the "nature" of probability, and choices among ۲ databases, and within the same data base
- the choice of the modelling (e.g. by Fault tree method) for hazards identification, for ۲ structuring the quantification of the event frequencies.
- the choice and the use of the physical models (which only in part derive from epistemic ٠ uncertainty)
- the bias introduced by the context (e.g. in a regulatory environment which in some way ٠ prescribes certain parameters, models)
- the completeness of the analysis, which can derive from practical constraints but also ۲ choices in the boundaries
- the basic experience of the analysts and his operational background etc. Lack of ۲ knowledge/misunderstandings about plant lay-out and operation







THANK YOU FOR YOUR ATTENTION



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